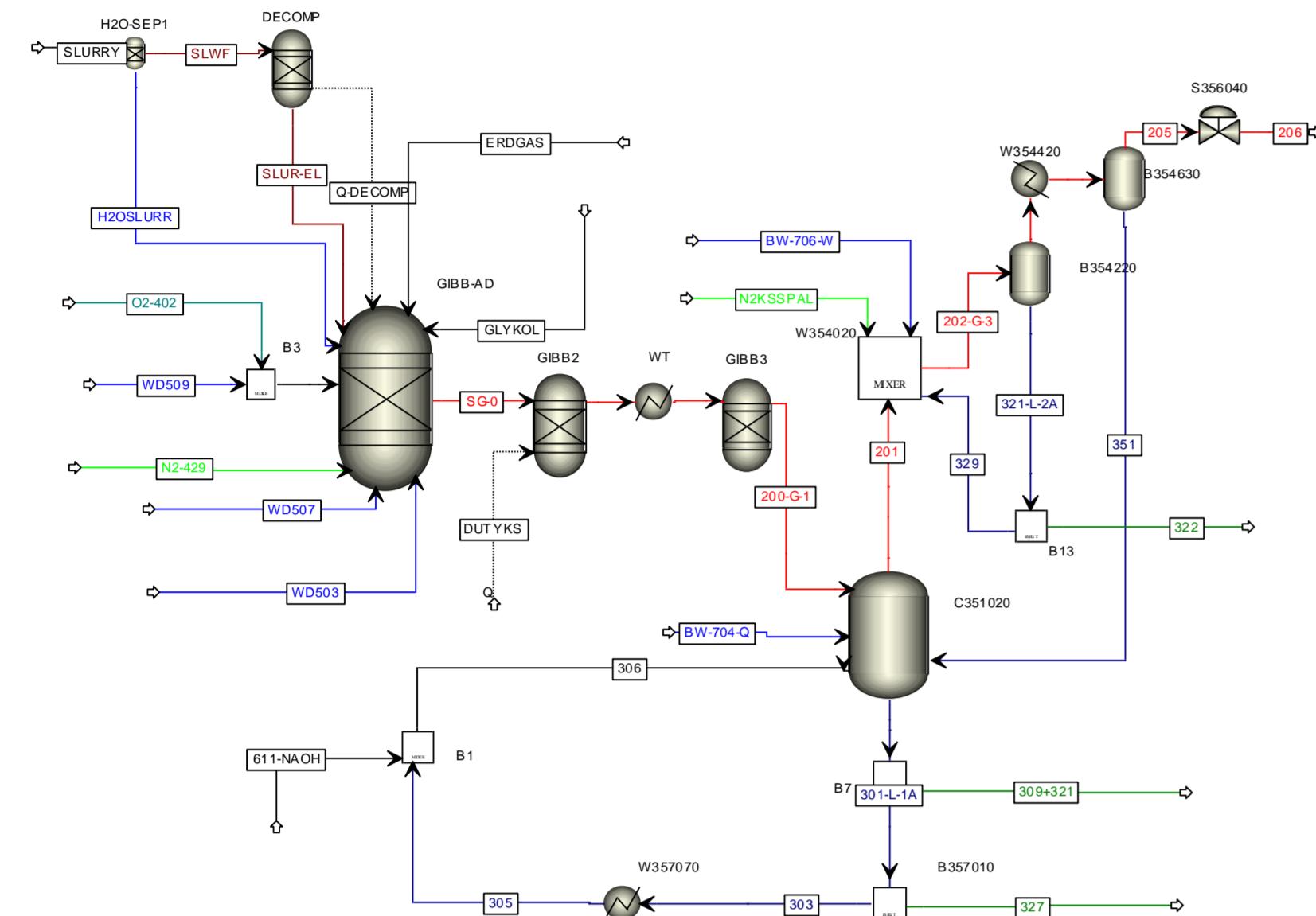


Modeling / Balancing for Entrained Flow Gasification

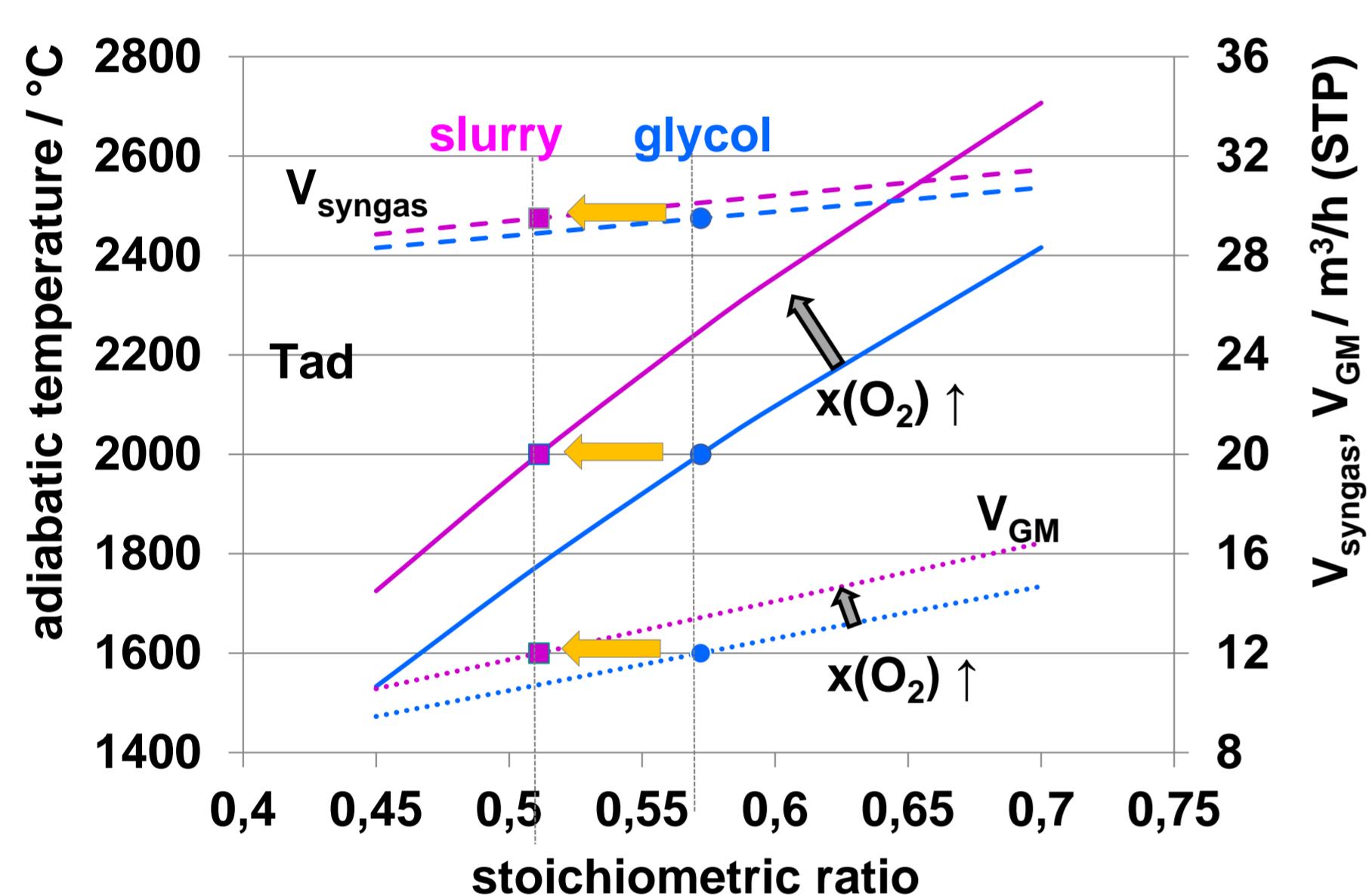
Ulrike Santo, Maximilian Dammann, David Böning, Thomas Kolb

Flowsheet Simulation

Reactor / process models of REGA and bioliq®



- Automated data transfer PCS-Excel-simulation
- Design and validation of experiments for REGA and bioliq® EFG



Fuel variation with constant temperature, residence time and flow field at REGA

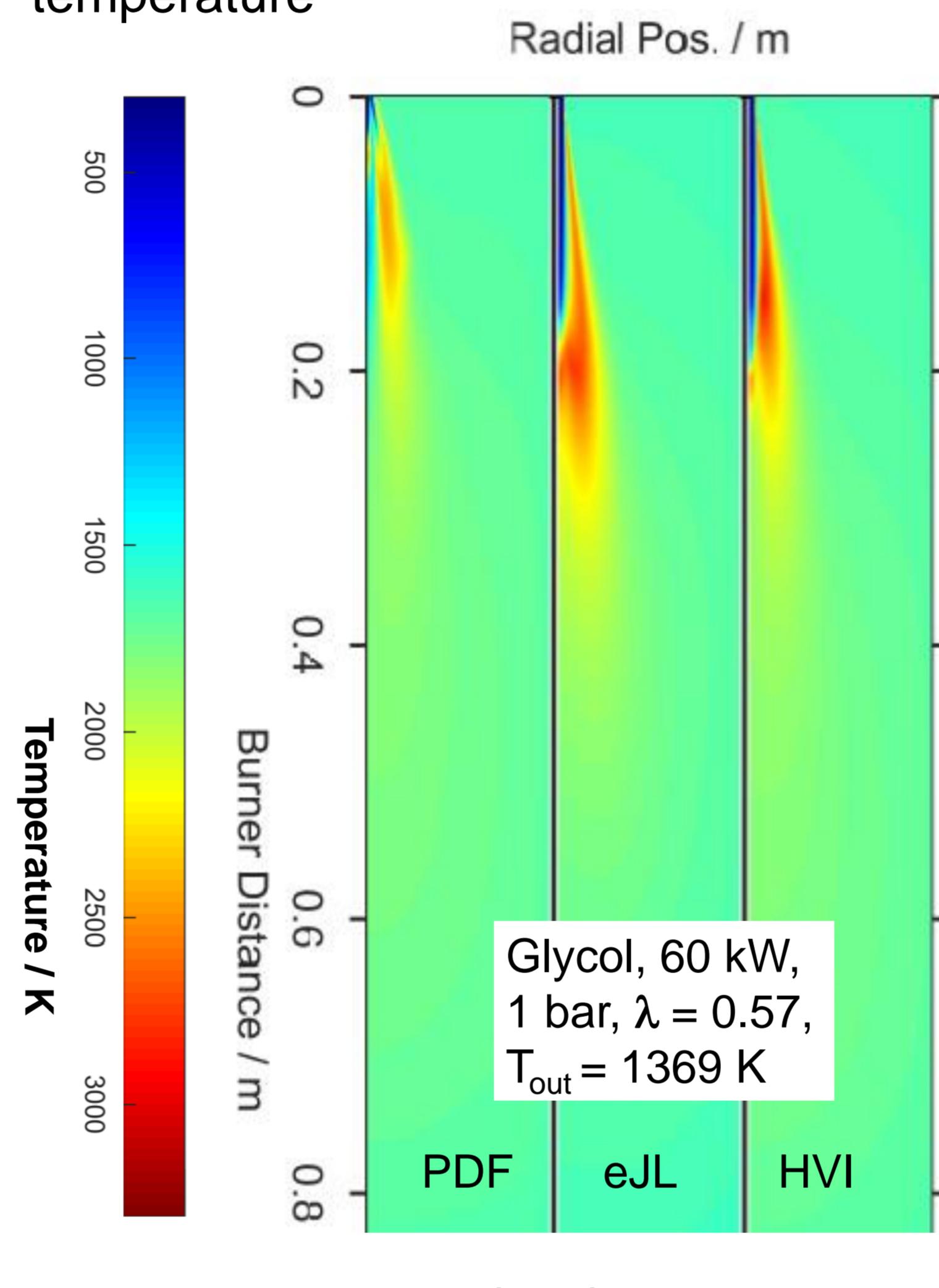
Numerical Simulation

CFD Simulation of EFG using RANS

- Gas phase reaction kinetics: EDC + global reaction mechanism
- Heterogeneous kinetics of char
- Slag: wall film model

Atmospheric REGA simulation

Influence of gas phase kinetics on temperature

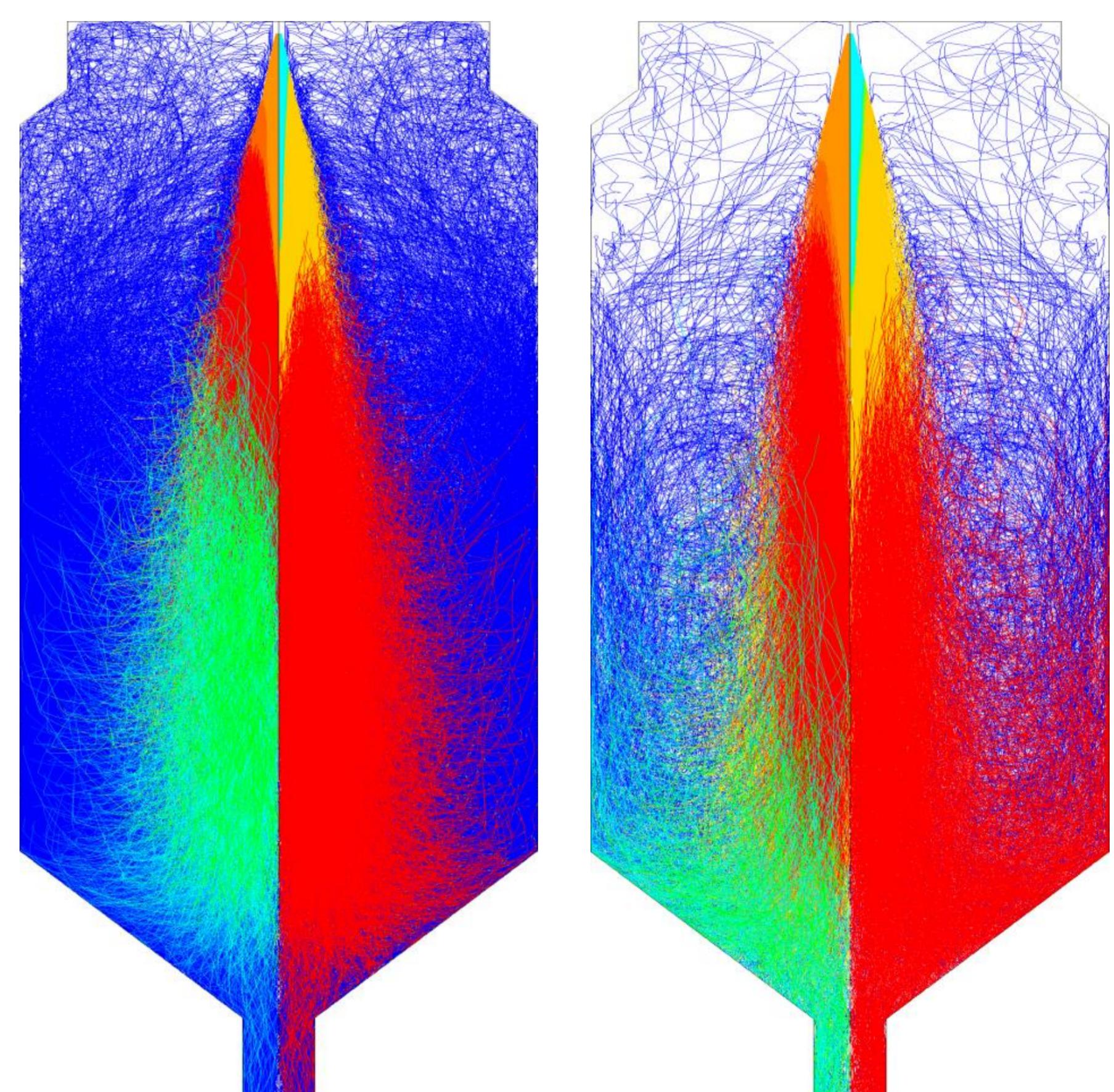


M. Mancini et al. Fuel (2018), submitted

Pressurized bioliq® simulation

Influence of particle size on conversion

100 µm droplets 200 µm



Left: Carbon in coke

High carbon content
Low carbon content

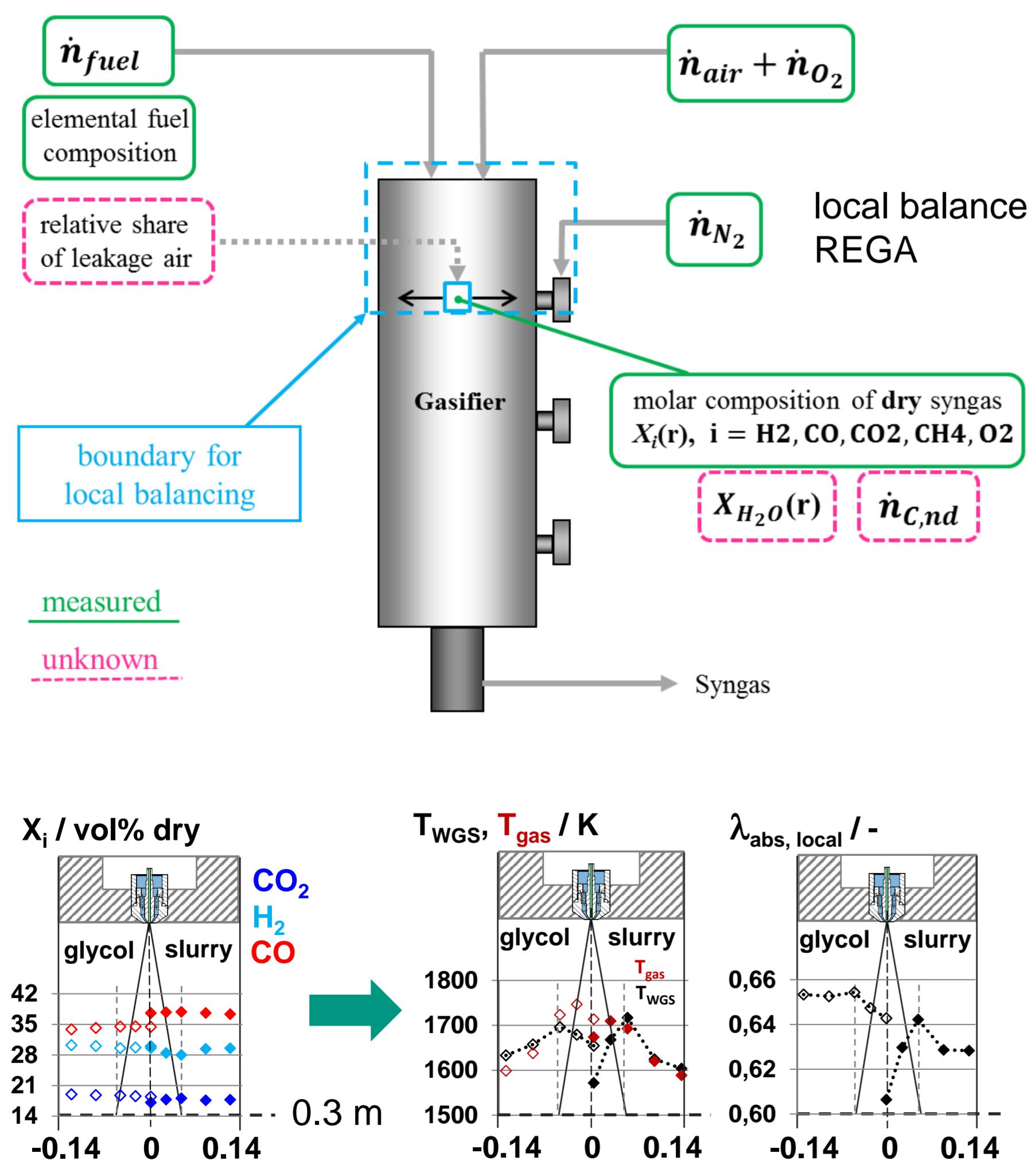
Droplet diameter	Solid diameter	C-Conversion
100 µm	63 µm	100 %
200 µm	125 µm	92 %

Slurry (30% solids), 5 MW, 40 bar, $\lambda = 0.56$, $T_{ad} = 2381$ K

Local / Global Balancing

Global and local balancing of gasification experiments at REGA, bioliq®

- calculation of missing data (leakage air, X_{H2O} , ...)
- calculation of characteristic parameters CC, λ , T_{WGS} , ...



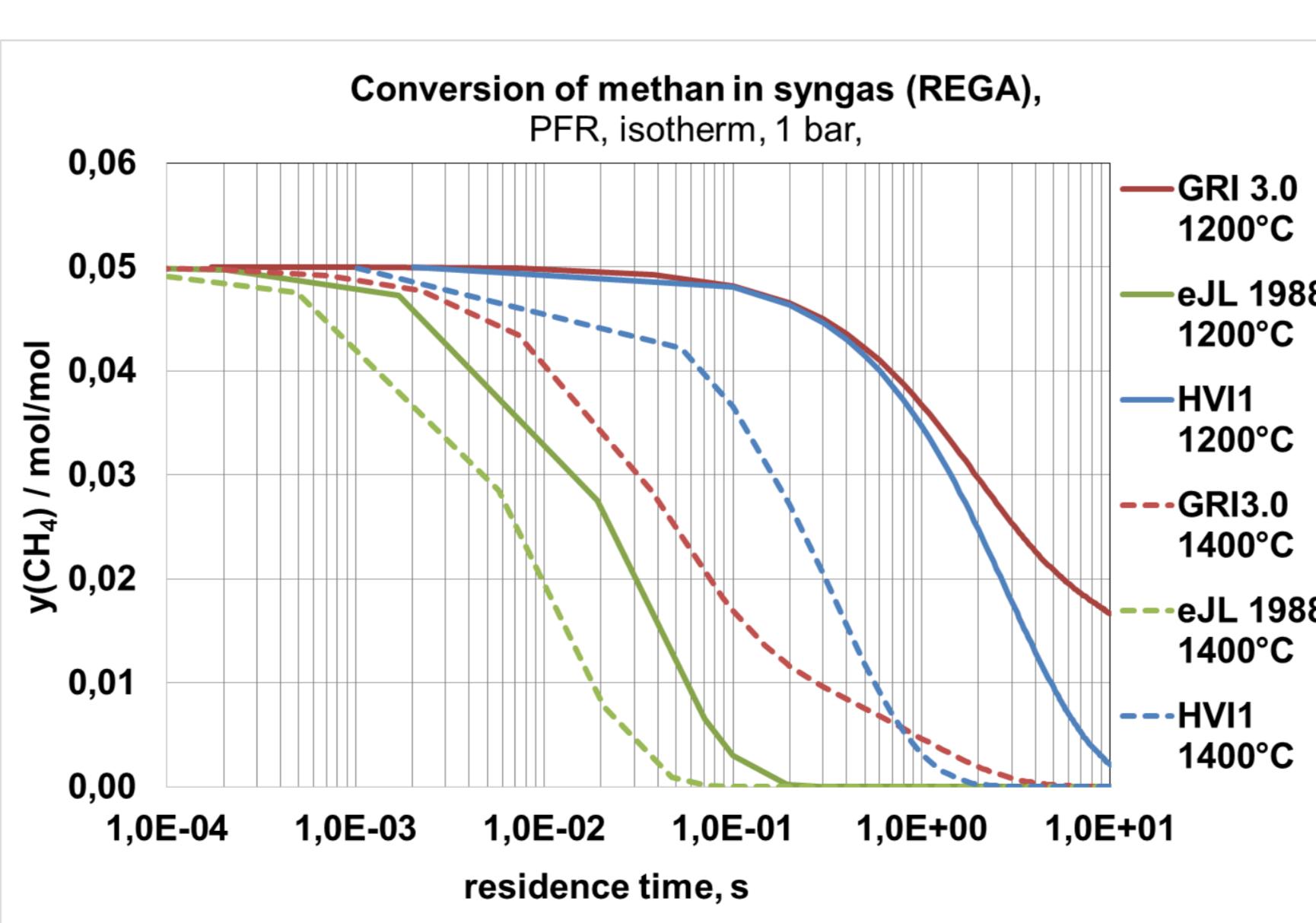
S. Fleck; et al.: Fuel 217 (2018) 306-319

Gas-Phase Kinetics

6 reactions gas phase HVI mechanism derived

- (1) decomposition of fuel at high heating rates
- (2) syngas oxidation in flame zone
- (3) WGS and reforming of hydrocarbons downstream

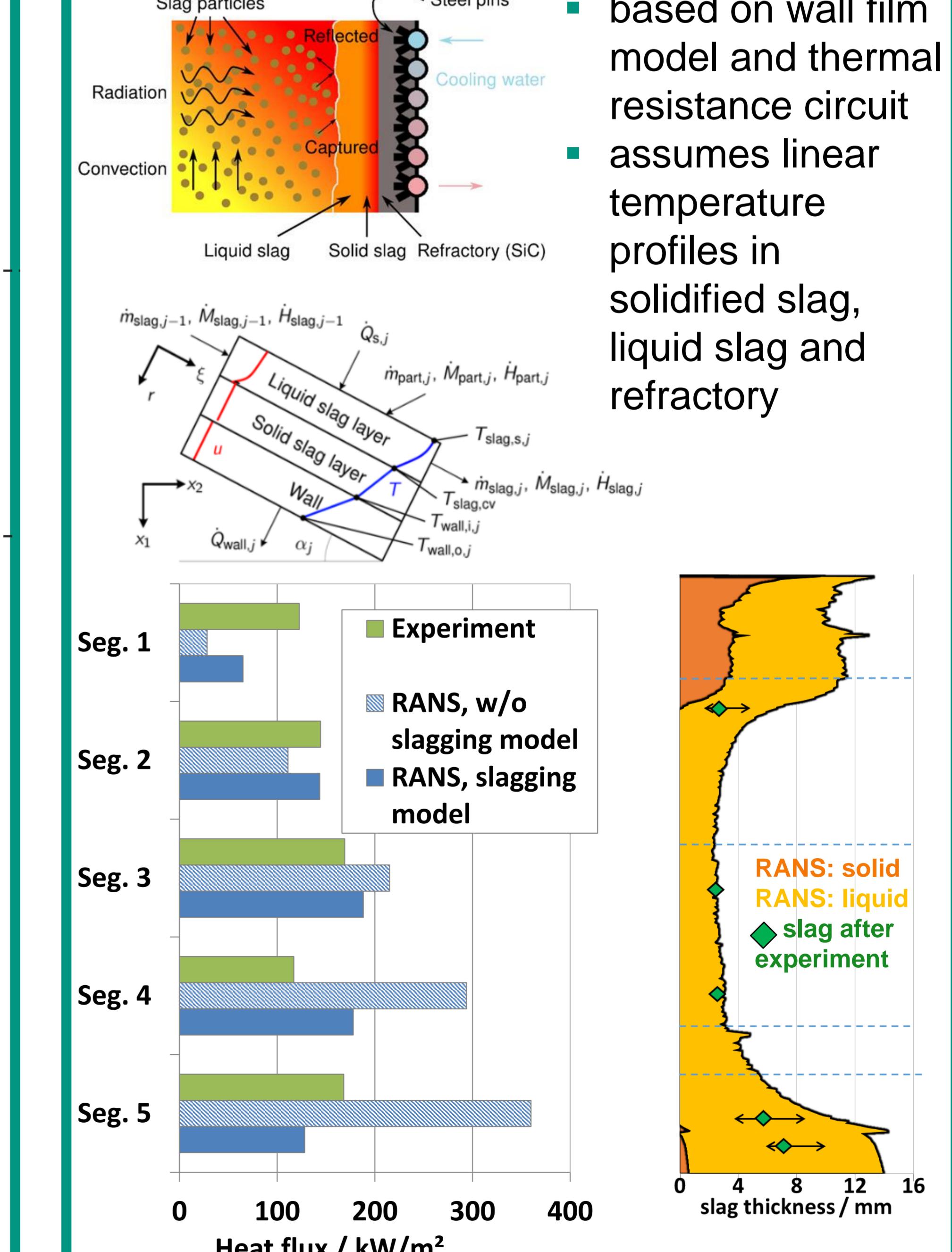
Validation of HVI mechanism versus detailed mechanisms
- GRI3.0 (2) + (3),
- DLR (1)



M. Mancini et al. Fuel (2018), submitted

Slagging Model

- based on wall film model and thermal resistance circuit
- assumes linear temperature profiles in solidified slag, liquid slag and refractory



Seibold et al., Fuel 197 (2017)